

ated)

March 10, 1997 -

Mr. Jerome M. Curtin
Compliance Officer
CERCLA Cost Recovery Section (3HW12)
U.S. Environmental Protection Agency
841 Chestnut Building
Philadelphia, Pennsylvania 19107

Dear Mr. Curtin:

These responses have been prepared by John T. Lucey, Jr., who was the Chester Project Manager responsible for working with Breslube-Penn in 1985. Mr. Lucey reviewed the enclosed documents, but did not consult with anyone in the proparation of these responses.

- 1. Chester Engineers provided engineering services and analytical laboratory services to Breslube-Penn. These services were provided to characterize their wastewater streams, to perform treatability studies, and to prepare an application requesting service for industrial wastewater discharge to the Moon Township Municipal Authority. The work was performed for Mr. Ahsen Yelkin, Vice President of Operations and Mr. Joseph Chalhoub, President. The facilities and its operations are described in the enclosed application.
- 2. We only know what is stated in Response No. 1. Copies of business cards for the referenced persons are enclosed.
- 3. The documents are enclosed and are described in Response No. 1.
- 4. All information available is enclosed.
- 5. Breslube employees are addressed in Responses 1 and 2. Mr. Robert Helwick and Mr. John Schrader, both employees of Chester Engineers, were responsible for the laboratory analyses and treatability studies. Chester point of contact will be John T. Lucey, Jr., Chester Engineers, Inc., Cherrington Corporate Center, 600 Clubhouse Drive, Pittsburgh, Pennsylvania 15108-3195; phone number: 412-269-5726.

600 Clubhouse Drive Pittsburgh, Pennsylvania 15108 412-269-5700; Fax 412-269-5749

- 6. Unknown.
- 7. Unknown.
- 8. All known information is enclosed.
- 9. No materials were provided by Chester.
- 10. No materials were provided by Chester.
- 11. The only authorities with whom we interacted were the Moon Township Municipal Authority and Coraopolis Municipal Sanitary Authority, both as described in the enclosed documents.
- 12. See enclosed.
- 13. None are known.
- 14. None are known.
- 15. None are known.
- None are known.
- 17. Not relevant to our services provided.
- 18. No such predecessors in our business.
- 19. None are known relative to their activity at the Breslube site.
- 20. None are known.
- 21. All information which we have been exposed to relative to the Breslube site is enclosed.

Mr. Jerome M. Curtin U.S. EPA March 10, 1997 Page 3

- 22. Not relevant.
- 23. None are known.

Very truly yours,

John T. Lucey, Jr., P.E.

President & COO

JTL/kak/3210

Enclosures

GENERAL ORDER ENTRY FORM

ORDER ENTRY NO. 3492-		URCHASE IGREEMEN	ORDER NO	1. <u>619</u> 1/8/85	PROPOSAL N	·	585-03-05
CONTRACT DATE		TART DA		18135	-	DATE 3/3	10/05
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DEPARTMENT: (S, C) O, R				TOTAL SALE VALU	IE \$	6,000	
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		MAN H TO COM					
LABOR:	<u>Ho</u>	ours	Cost	EXPENSES:			Cost
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Technician III	(28) •			Telephone		(440) _	
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Total Labor	_/	36 \$	3800	TOTAL LABO	OR AND EXPE	NSES \$	3850, -
CLIENT PERSONNEL IN CHA	DCE ·	:- :		ΔΟΙ	PROVALS		DATE
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·	:				•	•	/

1/85

for filing in contract file

Maureen D. McFalls Attorney At Law

903 Standard Life Building 345 Fourth Avenue Pittsburgh, PA 15222 (412) 765-2605 Bob Helweek

Demanstrator New To Stop Work It Fayment anuary 16, 1987 Not Recieved IN REASONAGE

PEREND - THIS WENT ON MUCH TOO LONG.

AF-1/30

Anthony Lisanti The Chester Engineers P.O. Box 9356 Pittsburgh, PA 15225

Dear Tony:

I spoke last week with the Controller of Breslube Enterprises, Mr. Ernie Trompke, regarding payment of Chester's outstanding Breslube-Penn, Inc. invoices.

Mr. Trompke informed me that he is in receipt of copies of all the outstanding invoices and adknowledges the amount owing at \$20,445.35. Breslube has offered to pay 33 1/3 cents on the dollar to all its creditors, and is willing to make the same offer to 'hester. As you know, the company has ceased all operations and does not have sufficient assets to cover its liabilities. I told Mr. Trompke I would transmit his offer to you and let him know your response. Even if Chester decides to accept the offer, I'm not certain that Breslube can pay one-third immediately, however, Trompke indicated that he would discuss this matter with the president of Breslube as soon as possible and pass such information on to me.

Please let me know how you would like me to proceed. Telephoned 1/27

proceed up partial payment agreement if paid within Earlys

-It not file legal claim whall costs.

Sincerely,

Maureen D. McFalls, Esq.

. MMF/1c

cc: Alfred Baily R. A. Radish



Bres Lure - Penn Inc.

84 MONTOUR ROAD, CORAOPOLIS, PENNSYLVANIA 15108

TEL (412) 284-4280 **TELEX 00902977**

February 2, 1987

The Chester Engineers P.O. Box 9356 Pittsburgh, Pennsylvania 15225

Attention: John T. Lucey, Jr.

Dear Mr. Lucey:

As you may know, BresLube Penn, Inc., has experienced considerable financial difficulties. We appreciate the patience many of our creditors have demonstrated.

To enable us to discharge balances currently owed by BresLube Fenn, we are asking creditors to accept the following payment arrangement:

Our records show that you are owed \$ 20,400.00. Under our proposal, you would be paid \$ 6.800.00 as a complete discharge of all claims you may have against Breslube Penn, Inc.

If this arrangement is satisfactory, please indicate below.

Yours very truly,

Emil Troughe

Ernie Trompke

Accepted with understanding we will receive the payment of \$6,800.00 within sixty (60) days of date of acceptance of offer.
Agreed and accepted this Zh day ZEB

Twent , V.P.

c: Maureen McFalls

LABORATORY ORDER ENTRY FORM

CLIENT NAME BRESLUBE ADDRESS BY NON (For Billing CORAD ROLL Purposes) DESCRIPTION ANALYSES CONTRACT STATUS REPORT (Yes PD EXPENSES TO BE BILLED AT PROJECT MANAGER JOHN	START DATE - FENN INC. TOUR ROAD -15 PA 15708 OF IND WASTEUM -NO) COST OR + 15 %	2/18/85 COMPLETION DATE PHYSICAL LOCATE COMPOSITION DATE CONTRACTED PD Billing Rate	TION OF PROJECT: IS ACT PO te No Baser 7.8 ELL VALUE:
	MAN HOURS	TOTAL SELL VALUE	
	TO COMPLETE		
LABOR:	Hours Cost	EXPENSES:	Cost
Chief Technical Consultant (2) Engineer Manager III (3) Engineer Manager II (4) Engineer Manager I (5) Engineer/Scientist IV (9) Engineer/Scientist III (10) Engineer/Scientist II (11) Engineer/Scientist II (12) Technician IV (27) Technician III (28) Technician II (29) Technician I (30) Total Labor	54	Transportation (300 Miscellaneous Travel (301 Per Diem (302 Photocopies (340 Postage (340 Expendable Supplies (340 Co. Vehicle Mileage (340 Sample Shipment (340 Equipment Rental (350 Telephone (440 Subcontractors (620 Total Expenses TOTAL LABOR & EXPENSES	1)
CLIENT PERSONNEL IN CHARGE:	PROJE(CI MANAGER WAL WAL	DATE 2/19/85 = -19 75



AHSEN YELKIN

84 Montour Road Coraopolis, Penn. 15108 Phone (412) 264-4280 Telex 902977

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Breslube Enterprises P.O. Box 130 Bresleu, Ontario, Canada NOB 1M0

JOSEPH CHALHOUB, P.Eng.

Office (519) 648-2291 Control Room (519) 648-2204

he**Chester**Engineers

Ref. No. 3492-20

October 29, 1985

Moon Township Municipal Authority 1000 Beaver Grade Road Coraopolis, PA 15108

ATTN: Mr. Richard Zollinger

Gentlemen:

Re: Breslube-Penn, Inc.

As stated in our July 18, 1985 letter, we have conducted a program of additional sampling and treatability studies to provide you with the information that you had requested on the efficiency of the proposed pretreatment process. The program was conducted as follows:

- 1. Wastewater samples were collected on five different days (8/9, 8/13, 8/21, 8/23 and 8/29). Samples of the raw dehydration, emulsion breaking and coolant wastewaters were collected (referred to as °1 or primary treatment). In addition, the Breslube personnel neutralized and filtered samples of the dehydration, emulsion breaking and coolant wastewaters. The resultant filtrate was collected and referred to as °2 or secondary treatment. Both the coolant wastewater and the emulsion breaking wastewater are routinely treated on the Breslube site through the emulsion breaking process described in the original application.
- The collected samples were analyzed for pH, BOD5, freon extractables, phenolics, ammonia, cyanide, chromium, copper, lead, nickel and zinc.
- 3. The samples were then mixed in the proportions similar to those that would be expected in a pretrestment operation. This is, one part of emulsion breaking water with 1-1/2 parts of coolant water and 1-1/2 parts of dehydration water. The mixtures were allowed to sit in a quiescent state for five days. The oil was then skimmed off the top.
- 4. The remaining mixtures were then analyzed for the parameters listed above as well as volatile organic compounds.

- 5. Treatment of the mixtures was then performed in a 1000 mL glass beaker as follows:
 - a. neutralize with lime to pH 9; mechanically agitate for 15 minutes
 - b. add 10 mg/L of sodium sulfide and 1 gram/liter of activated clay and mix for 5 minutes
 - c. filter through 50 Whatman paper
- 6. The effluent was then analyzed for the parameters listed in 2. above.

The results of the program described above are enclosed. The results of the treatment of the secondary treatment wastewaters are provided for your information only. This practice will not be implemented. The proposed pretreatment process will remain as presented in the original application with the exception of the addition of 1 gram/liter of activated clay in the chemical treatment step. As can be seen in the enclosed results, the laboratory treatability study using this process with the raw wastewater produced the following effluent quality.

Ef	flu	ent	Qua	lity	

	Average	Maximum	Minimum
pH	8.5	8.5	8.4
BOD5, mg/L	2860	4200	1400
Freon Extractables, mg/L	36.6	57	13
Phenolics, mg/L PhOH	26.3	100	- 1.7
Ammonia, mg/L N	39	101	3.8
Cyanide, mg/L CN	less than 0.025	0.062	lesa than 0.01
Chromium, mg/L Cr	less than 0.01	0.01	less than 0.01
Copper, mg/L Cu	0.03	0.06	0.01
Lead, mg/L Pb	0.06	0.12 4-	0.01
Nickel, mg/L Ni	0.14	0.23	0.09
Zinc, mg/L Zn	0.16	0.26	0.07

The effluent produced in the laboratory met all of the previously reported effluent limitations for all but one borderline excursion on both ammonia and lead. A full scale operation with automatic pH control to maintain the pH at or near 9 can be expected to produce a more consistent quality effluent that would consistently meet the effluent limitations.

In response to your comments and those by the Allegheny County Health Department, we ran volatile organic compound analyses on several of the samples. The results of these analyses are also enclosed. Discharge of these compounds to a POTW is not specifically regulated by EPA for the Petroleum Refining Lube Subcategory. However, the concentrations of these compounds provides an indication of whether vaporized volatile compounds will be released in the sewer system. It can be noted that the concentrations of the various compounds are in each case well below their solubility in water. This does not preclude their volatilization and release to the atmosphere, when exposed to that atmosphere under the proper conditions. However, at these low concentrations and especially at the lower concentrations that will exist in the sewer system due to dilution, little volatilization can be expected. The solubility in water for the various compounds is listed in Attachment 1.

You will note that an analysis of the tank bottom drainings has not been included. Breslube has terminated the direct discharge of these and has been routing these drainings either through the dehydration or emulsion bresling systems. This practice would continue with pretreatment and discharge.

We trust that this provides you with the additional information that you have requested.

Very truly yours,

John T. Lucey, Jr., P.E.

JTL/pl

Attachment

cc: Breslube-Penn, Inc.

ATTACHMENT 1

SOLUBILITY OF RELEVANT VOLATILE COMPOUNDS

Source	Solubility (mg/L) at 20°C
Benzene	1,800
Chloroform .	8,200
1,1 Dichloroethane	5,500
1,2 Dichloroethane	8,690
1,1 Dichloroethylene	400
Ethylbenzene	152
Methylene Chloride	20,000
Tetrachloroethylene	150-200
Toluene	535 @ 25°
1,2 Trans-Dichloroethylene	600
1,1,1 Trichloroethane	4,400
Trichloroethylene	1,100

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Laboratory Analysis Report

Corsopolis, Pennsylvania BresLube-Penn, Inc.

Analyses

Samples Received: 8/09/85 Report Date:

Dehydration Water Secondary Treatment	6445 8/8/85	4.0 4,740 23 24 146 0.021 0.021 0.15 0.10 0.10
Dehydration Water Primary Treatment	6444 8/8/85	5,800 132 132 159 77 0.046 0.03 3.7
Emulsion Breaking Water Secondary Treatment	6443 8/8/85	5.1 4,950 81 173 0.02 0.01 0.02 2.2 0.40
Emulaion Breaking Water Primary Treatment	6442 8/8/85	6.0 7,685 353 21 100 0.026 0.06 1.5 3.3 0.45
Source	Log No. 85- Date Collected	pH BOD5, mg/L Freon Extractables, mg/L Freon Extractables, mg/L Phenolics, mg/L PhOH Ammonia, mg/L N Cyanide, mg/L CN Chromium, mg/L CL Copper, mg/L CL Lead, mg/L Pb Nickel, mg/L Pb Sinc, mg/L Zn

6446 8/8/85

0.017

0.06 0.01 2.2

0.35

Coolent

Water

after

Paulston

Broken

3492-90

Unless otherwise noted, analyses are in accordance with the methods and procedures outlined and approved by the Environmental Protection Agency and conform to quality assurance protocol.
 "Less-than" (<) values are indicative of the detection limit.

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Leboratory Analysis Report For

BresLube-Penn, Inc. Coreopolis, Pennsylvania

Analyses

Samples Received: 8/13/85 Report Date: 9/16/85				
Source	Emulsion Breaking Water Primary Treatment	Emulsion Breaking Water Secondary Treatment	Dehydration Water Primary Treatment	Dehydration Water Secondary Treatment
Log No. 85-	9959	1959	6562	6563
Hd	5.8	4.9	3.6	4.3
BODs. mg/L	8,310	4,170	5,633	6,950
Freon Extractables, mg/L	846	•	870	28
Phenolics, mg/L PhoH	21	71	ដ	11
Ammonia, mg/L N	57	160	0.68	04
Cyanide, mg/L CN	(0.01	(0.01	0.85	0.28
Chrostum, mg/L Cr	0.11	0.03	(0.01	(0.01
Copper, mg/L Cu	1.6	90.0	0.07	0.10
Lead, mg/L Pb	2.3	3.6	13	2.0
Mickel, mg/L Ni	0.47	0,36	6.07	0.05
Zinc, mg/L Zn	1.2	0.20	1.9	69.0

Water

Coolent

Coolant Water Primary

Treatment

Treatment

6565

6564

60.01 0.02 0.06 0.07 0.32

111 0.25 3.6 0.062 0.12 0.08 0.39

17 0.69 1.8

466

1.8 993

Unless otherwise noted, analyses are in accordance with the methods and procedures outlined and approved by the Environmental Protection Agency and conform to quality assurance protocol.
 "Less-than" (<) values are indicative of the detection limit.

BPDR 0002797

Laboratory Analysis Report For

Breslube-Penn, Inc. Coraopolis, Pennsylvania

Analyses

Samples Received: 8/09/85 Report Date: 9/16/85

	Composite of			•
	1 Part	85-6711		85-6713
	85-6442	Treated		Treated
	. 3 Parts	with Line		with Lime
a ²	85-6444	to pH 9.0		to pH 9.0
	Subnate	at.d 10 mg/L		And 10 mg/L
	after 5 days	Sulfide added		Sulfide added
	Quiescent	Filter through		Filter through
Source	Settling	5 n Filter	85-6445	5 p Pilter
Log No. 85-	6711	6712	6713	6714
Н	. 8.4	8.4	4.5	8.8
BODS, mg/L	5,450	4,200	4,600	4,400
Freon Extractables, mg/L	182	57	451	28
Phenolics, mg/L PhOH	101	100	101	101
Ammonia, mg/L N	. 62	. 62	234	159
Cyanide, mg/L CN	0.032	0.032	0.028	0.029
Chromium, mg/L Cr	0.01	<0.01	0.0	10.0
Copper, mg/L Cu	0.37	90.0	0.01	0.02
Lead, mg/L Pb	0.54	0.12	0.30	0.18
Nickel, mg/L Ni	0.08	0.13	0.12	0.17
21nc, mg/L 2n	0.38	0.0	0.11	0.02

Unless otherwise noted, analyzes are in accordance with the methods and procedures outlined and approved by the Environmental Protection Agency and conform to quality assurance protocol.
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Laboratory Analysis Report For BresLube-Penn, Inc. Coraopolis, Pennsylvania

Analyses

Samples Received: 8/13/85 Report Date: 9/16/85

*	- 1	85-6715	:	85-6717
•	Composite of	Treated	Composite of	Treated
	1 Part	with Line	1 Part	with Line
	85-6566	to pH 9.0	85-6567	. to pH 9.0
•	1.5 Parts	and 10 mg/L	1.5 Parts	and 10 mg/L
	85-6562	Sulfide added	85-6563	Sulfide added
	1.5 Parts	Filter through	1.5 Parts	Pilter through
Source	83-6564	5 p Filter	85-6565	5 u Filter
Log No. 85-	6715	6716	671.7	6718
Hd	4°	80°	5.0	9.0
BOD5, mg/L	3,350	3,500	5,400	3,500
Freon Extractables, mg/L	280	35	20	. 20
Phenolics, mg/L PhOH	9.6	9.5	9.7	9.5
Amount, mg/L N	- 11 .	11	=======================================	=
Cyanide, mg/L CN	0.062	0.062	0.055	0.052
Chromium, mg/L Cr	0.07	0.01	(0.01	(0.01
Copper, mg/L Cu	96.0	0.03	0.05	0.01
Lead, mg/L Pb	0.76	0.10	0.13	0.08
Nickel, mg/L Ni	0.30	0.23	0.19	0.21
Zinc, mg/L Zn	2.3	0.26	0.70	0.13

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Laboratory Analysis Report For

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Bres-Lube Penn, Inc. Coraopolis, Pennsylvania

Analyses

Samples Received: 8/29/85
Report Date: 9/18/85

Source	Coolant Water 1 Treatment	Coolant Mater	Raulaion Braaking Water 1 Treatment	Emulsion Breaking Water '2 Treatment	Debydrated Water 1 Treatment	Dehydrated Mater 2 Treatment
Log No. 85- Date Collected	7099 8/29/85	7100 8/29/85	7101	7102 8/29/85	7103 8/29/85	7104
# 4	1.0	2.5	1.0	. 4.	9.9	9.9
BODs - ms/L	1,305	330	2,270	4,893	975	009
Freom Extractables, me/L	62	2.4	3	26	£	21
Phenolics me/L Phob		0.092	5.4	11	3.4	3.8
Amenda me/L H	0.82	0.91	11	167	. 20	11
Cvanide, mg/L CN	(0.0)	(0.0)	0.01	0.01	(0.0)	(0.01
Chromium, me/L Cr	0.30	0.01	0.30	(0.01	(0.01	<0.01
	0.11	0.07		0.02	90.0	0.03
Land me/L. Ph	5.2	0.13	. 3.7	(0.01	0.16	¥.0
Mickel, me/L 21	0.47	0.07	0.43	0.24	10.01	0.01
Zinc, mg/L 2n	8.6	0.31	7.5	01.0	0.23	3.3

3462-68

Unless otherwise noted, analyses are in accordance with the methods and procedures outlined and approved by the Environmental Protection Agency and conform to quelity esqurance protocol.
 "Less-then" (<) values are indicative of the detection limit.

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Samples Received: Report Date:

Laboratory Analysis Report For

Bres-Lube Pann, Inc. Corzopolis, Pannsylvania

Analyees

Source	1 Part 85-7101 1.5 Parts 85-7099 1.5 Parts 85-7103 Sectled for five days and Oil Skimmed	Log No. 85-7195, pH 8.5 with Lime and 10 mg/L Sulfide and 1 g/L Activated clay added. Filter through 5p Filter	1 Part 85-7102 1.5 Parts 85-7104 1.5 Parts 85-7104 8attled for five days and Oil Skimmed	Log No. 85-7197, pH 8.5 with Lime and 10 mg/L Sulfide and 1 g/L Activated clay added. Filter through 5p Filter
Log No. 85-	7195	7196	7197	7198
3 0	1:1	6.5	4.7	8.5
Bobs, mg/L	1,500	1,800	1,380	1,620
Freon Extractables, mg/L	37	13	16	13
Phenolics, mg/L PhoH	2.3	1.7	3.5	3.1
Ammonia, mg/L N	12	3.8	94	45
Cyanida, mg/L CN	(0.0)	(0.0)	(0.0)	(0.01
Chromium, mg/L Gr	0.14	10.0>	(0.0)	(0.01
Copper, mg/L Cu	0.63	0.01	0.03	. <0.01
Lead, mg/L Pb	2.6	0.03	5 .0	10.0>
Mickel, mg/L Mi	0.27	0.10	0.05	0.03
Zinc, mg/L Zn	5.3	0.15	0.12	0.02

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Laboratory Analysis Report For

BresLube-Penn, Inc. Corsopolis, Pennsylvania

Volatile Compounds

Complex Decales de	Volatile Con	apounds		
Samples Received:				
Report Date: 9/16/85	Composite		_	
	of 1 Part ,		Composite	Composite
	85-6442	_	of 1 Part	of 1 Part
	3 Perts	Composite	85-6566	85-6567
	85-6444	of 1 Part	1.5 Parts	1.5 Parts
	Subnate	85~6443	85-6562	85 -6 563
·	after 5 days	3 Parts	1.5 Parts	1.5 Parts
Source	Settling'	85-6445	85-6564	85-6565
Log No. 85-	6711	6713	6715	6717
Acrolein, pg/L	<10	<10	<10	<10
Acrylonitrile, µg/L	<10	<10	<10	<10
Bensene, µg/L	500	232	1,326	167
Bromoform, ug/L	· <10	₹10	<10	<10
Carbon Tetrachloride, µg/L	<10	<10	<10	<10
Chlorobensene, ug/L	<10	<10	<10	<10
Chlorodibromomethane, µg/L	<10	<10	<10	<10
Chloroethane, ug/L	<10	<10	<10	<10
2-Chloroethylvinyl Ether, µg/L	<10	<10	<10	<10
Chloroform, ug/L	<10	<10	<10	<10
Dichlorobromomethane, ug/L	<10	<10	<10	<10
1,1-Dichloroethane, µg/L	53	28	33	· <10
1,2-Dichloroethane, pg/L	<10	25	<10	<10
1,1-Dichloroethylene, µg/L	<10	<10	<10	<10
1,2-Dichloropropane, ug/L	<10	<10	<10	<10
cis-1,3-Dichloropropene, µg/L	<10	<10	<10	<10
trans-1,3-Dichloropropene, µg/L	<10	<10	<10	<10
Ethylbenzene, ug/L	105	<10	157	<10
Methyl Bromide, µg/L	<10	<10	<10	<10
Methyl Chloride, ug/L	₹10	<10	<10	<10
Mathylane Chloride, µg/L	1,555	444	1,773	378
. 1,1,2,2-Tetrachloroethene, ug/L	<10	<10,	<10	<10
Tetrachloroethylene, ug/L	140	<10	77	<10
Toluens, µg/L	1,350	341	3,130	230
1,2-Trans-Dichloroethylene, µg/L	⟨10	<10	1,238	179
1,1,1-Trichloroethane, ug/L	669	. 277	479	49
1,1,2-Trichloroethane, ug/L	<10	<10	₹10	<10
Trichloroethylene, µg/L	47	17	78	<10
Vinyl Chloride, µg/L	<10	<10	<10	<10
ASON AUTHET ARE HELD			.=•	_

Unless otherwise noted, analyses are in accordance with the methods and procedures outlined and approved by the Environmental Protection Agency and conform to quality assurance protocol.

^{. &}quot;Less-than" (<) values are indicative of the detection limit.

A Division Of The Chester Engineers PO Bas 1988 Passburgh Panaghana 13228 Page 1418 200-2700

Laboratory Analysis Report For

BresLube-Penn, Inc. Coraopolis, Pennsylvania

Volatile Compounds

Samples Received: Report Date: 9/17/85

Source	omposite of 85-6947 85-6849 and 85-6851 Settled For 5 days	1.5 Parts 85-6848 1.5 Parts 85-6850 1 Part 85-6852 Settled For 5 days	Gomposite of 85-6908 85-6910 and 85-6912 Settled For 5 days	Composite of 85-6909 85-6911 and 85-6913 Settled For 5 days
Log No. 85-	6984	6986	7039	7041
Acrolein, ug/L	<10	<10	<10	· <10
Acrylonitrile, µg/L	<10	<10	<10	<10
Benzene, µg/L	73	63	461	443
/Bromoform, µg/L	<10	<10	<10	<10
Carbon Tetrachloride, µg/L				
Chlorobenzene, µg/L	<10	<10	<10	<10
Chlorodibromomethene, µg/L	<10	<10	<10	<10
Chloroethane, µg/L	<10	<10	<10	<10
2-Chloroethylvinyl Ether, ug/L	· · <10	<10	<10	<10
Chloroform, µg/L	13	296	10	605
Dichlorobromomethane, µg/L	<10	<10	<10	<10
l,l-Dichloroethame, µg/L	27	11	65	<10
1,2-Dichloroethane, µg/L	<10	11	70	84
1,1-Dichloroethylene, ug/L	<10	<10	12	<10
1,2-Dichloropropane, ug/L	<10	<10	<10	<10
cis-1,3-Dichloropropene, µg/L	<10	<10	<10	<10
trans-1,3-Dichloropropene, µg/	/L <10	<10	<10	<10
Ethylbenzene, µg/L	16	<10	53	<10
Methyl Bromide, µg/L	<10	<10	<10	<10
Hethyl Chloride, µg/L	<10	<10	<10	<10
Methylene Chloride, µg/L	90	63		10
1,1,2,2-Tetrachloroethane, ug/	/L <10	<10	<10	<10
Tetrachloroethylene, µg/L	14	<10	78	10
Toluene, µg/L	251	157	1,100	750
1,2-Trans-Dichloroethylene, μ	g/L 18	<10	38	31
1,1,1-Trichloroethane, µg/L	171	114	<10	572
1,1,2-Trichloroethane, µg/L	<10	<10	<10	<10
Trichloroethylene, µg/L	<10	<10	78	55
Vinyl Chloride, µg/L	<10	<10	<10	<10

The Chaster Engineers

P.O. Box 9354 Presourch Pennsylvania 15225 Priena: (412) 255-5700

Laboratory Analysis Report

Bres-Lube Penn, Inc. Coraopolis, Pennsylvania

Samples Received:

Volatile Compounds

Report Date: 9/17/85

Source For 5 days For 5 days	, v	Composite of 85-7101 85-7099 and 85-7103 Settled	Composite of 85-7102 85-7100 and 85-7104 Settled
Acrolein, μg/L	Source	For 5 days	For 5 days
Acrylonitrile, μg/L βanzene, μg/L βanzene, μg/L (10 βanzene,	Log No. 85-	7195	7197
Acrylonitrile, μg/L βanzene, μg/L βanzene, μg/L (10 βanzene,	Acrolein, ug/L	<10	<10
Benzene, μg/L 208 18 Bromoform, μg/L C10		<10	<10
Carbon Tetrachloride, μg/L Chlorobenzene, μg/L Chlorodibromomethane, μg/L Chlorodibromomethane, μg/L Chloroethane, μg/L Chloroethylvinyl Ether, μg/L Chloroform, μg/L Dichlorobromomethane, μg/L L Cl0 Cl0 Cl0 Cl0 Cl1 Cl1 Cl1 Cl1		208	18
Chlorodibromomethane, ug/L Chlorodibromomethane, ug/L Chlorodibromomethane, ug/L Chloroethane, ug/L 2-Chloroethylvinyl Ether, ug/L Chloroform, ug/L Dichlorobromomethane, ug/L 115 89 Dichlorobromomethane, ug/L 1,1-Dichloroethane, ug/L 1,2-Dichloroethane, ug/L 1,2-Dichloroethane, ug/L 1,2-Dichloroethane, ug/L 1,2-Dichloropropane, ug/L 1,2-Dichloropropane, ug/L 1,2-Dichloropropane, ug/L 1,2-Dichloropropane, ug/L 1,3-Dichloropropane, ug/L 10 Cis-1,3-Dichloropropane, ug/L 10 Cibylbenzene, ug/L 10 Mathyl Bromide, ug/L 10 Mathyl Bromide, ug/L 10 Mathylene Chloride, ug/L 10 Clo Mathylene Chloride, ug/L 11,1-Z-Tertrachloroethane, ug/L 11,1-Trichloroethane, ug/L 11,2-Trichloroethane, ug/L 11 12 130 130 131 130 131 130 131 130 131 130 131 130 131 130 131 130 131 130 131 130 131 131		<10	<10
Chlorodibrosomethane, µg/L Chloroethane, µg/L Chloroethane, µg/L Chloroethylvinyl Ether, µg/L Chloroform, µg/L Chloroform, µg/L Chloroform, µg/L Chloroform, µg/L Dichlorobrosomethane, µg/L 115 89 Dichlorobrosomethane, µg/L 1,2-Dichloroethane, µg/L 1,1-Dichloroethane, µg/L 1,1-Dichloroethylene, µg/L 1,1-Dichloropropene, µg/L Cl0 Cl0 Cl0 Cl2-Dichloropropene, µg/L Cl0 Cl0 Cl0 Cl0 Cis-1,3-Dichloropropene, µg/L Cl0 Cl0 Cl0 Cl0 Cl0 Ethylbenzene, µg/L Actio Cl0 Cl0 Cl0 Methyl Bromide, µg/L Actio Cl0 Cl0 Hathylene Chloride, µg/L Cl0 Cl0 Cl0 Tetrachloroethylene, µg/L Cl0 Cl0 Cl0 Cl0 Cl0 Cl0 Cl0 Cl	Carbon Tetrachloride, µg/L	<10	<10
Chloroethane, μg/L 2-Chloroethylwinyl Ether, μg/L Chloroform, μg/L Dichlorobromomethane, μg/L 115 89 Dichlorobromomethane, μg/L 1,1-Dichloroethane, μg/L 1,2-Dichloroethylene, μg/L 1,2-Dichloropthylene, μg/L 1,2-Dichloropropene, μg/L Cio Cis-1,3-Dichloropropene, μg/L Cio Cis-1,3-Dichloropropene, μg/L Cio Cib-1,3-Dichloropropene, μg/L Cio Cin Cin Cin Cin Cin Cin Cin	Chlorobenzene, µg/L	<10	<10
2-Chloroethylvinyl Ether, μg/L Chloroform, μg/L Chloroform, μg/L Dichlorobromomethane, μg/L 1,1-Dichloroethane, μg/L 1,2-Dichloroethane, μg/L 1,1-Dichloroethylene, μg/L 1,2-Dichloropropane, μg/L 1,2-Dichloropropane, μg/L cis-1,3-Dichloropropane, μg/L cis-1,3-Dichloropropane, μg/L cis-1,3-Dichloropropane, μg/L trans-1,3-Dichloropropane, μg/L Ethylbenzene, μg/L Methyl Bromide, μg/L Methyl Bromide, μg/L Methyl Chloride, μg/L Methylene Chloride, μg/L Toluene, μg/L Toluene, μg/L 1,1,2-Trans-Dichloroethylene, μg/L 1,1,1-Trichloroethylene, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethylene, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethylene, μg/L		<10	<10
Chloroform, ug/L 115 89 Dichlorobromomethane, μg/L <10	Chloroethane, µg/L		· = •
Dichlorobromomethane, μg/L <10	2-Chloroethylvinyl Ether, µg/L		<10
1,1-Dichloroethane, µg/L 1,2-Dichloroethane, µg/L 1,1-Dichloroethylene, µg/L 1,1-Dichloropropane, µg/L cis-1,3-Dichloropropane, µg/L cis-1,3-Dichloropropane, µg/L cis-1,3-Dichloropropane, µg/L cis-1,3-Dichloropropane, µg/L cinc-1,3-Dichloropropane, µg/L cinc-1,3-Dichloropropane, µg/L cinc-1,3-Dichloropropane, µg/L cinc-1,0-Dichloropropane,	Chloroform, ug/L	115	89
1,2-Dichloroethane, μg/L 1,1-Dichloroethylene, μg/L 1,2-Dichloropropane, μg/L 1,2-Dichloropropane, μg/L cis-1,3-Dichloropropane, μg/L cis-1,3-Dichloropropane, μg/L cin-1,3-Dichloropropane, μg/L Ethylbenzene, μg/L Methyl Bromide, μg/L Methyl Bromide, μg/L Methyl Chloride, μg/L Hethylene Chloride, μg/L Toluene, μg/L Toluene, μg/L 1,2-Trans-Dichloroethylene, μg/L 1,1,2-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L 1,1,2-Trichloroethylene, μg/L 1,1,1-Trichloroethylene, μg/L	Dichlorobromomethane, µg/L		· - •
1,1-Dichloroaethylene, μg/L 1,2-Dichloropropane, μg/L cis-1,3-Dichloropropane, μg/L trans-1,3-Dichloropropene, μg/L Ethylbenzene, μg/L Methyl Bromide, μg/L Methyl Chloride, μg/L Tetrachloroethylene, μg/L 1,1,2-Trans-Dichloroethylene, μg/L 1,1,1-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L	1,1-Dichloroethame, µg/L		
1,2-Dichloropropane, μg/L cis-1,3-Dichloropropane, μg/L trans-1,3-Dichloropropene, μg/L Ethylbenzene, μg/L Methyl Bromide, μg/L Methyl Chloride, μg/L Hathylene Chloride, μg/L Tetrachloroethylene, μg/L Toluene, μg/L 1,2-Trans-Dichloroethylene, μg/L 1,1,2-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L			
cis-1,3-Dichloropropene, µg/L trans-1,3-Dichloropropene, µg/L Ethylbenzene, µg/L Methyl Bromide, µg/L Methyl Chloride, µg/L Hathylene Chloride, µg/L Toluene, µg/L 1,1,2-Trans-Dichloroethylene, µg/L 1,1,2-Trichloroethylene, µg/L 1,1,2-Trichloroethylene, µg/L 1,1,2-Trichloroethylene, µg/L 1,1,2-Trichloroethylene, µg/L Trichloroethylene, µg/L			
trans-1,3-Dichloropropene, μg/L Ethylbenzene, μg/L Methyl Bromide, μg/L Methyl Chloride, μg/L Hethylene Chloride, μg/L 1,1,2,2-Tetrachloroethane, μg/L Toluene, μg/L 1,2-Trans-Dichloroethylene, μg/L 1,1,1-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L 1,1,1-Trichloroethane, μg/L	1,2-Dichloropropane, μg/L	<10	<10
Ethylbenzene, μg/L <10	cis-1,3-Dichloropropens, µg/L	<10	<10
Methyl Bromide, μg/L <10			•
Methyl Chloride, μg/L <10	Ethylbenzene, µg/L		<10
Hethylene Chloride, μg/L 500 110 1,1,2,2-Tetrachloroethane, μg/L <10	Methyl Bromide, µg/L		7 -
1,1,2,2-Tetrachloroethane, μg/L Tetrachloroethylene, μg/L Toluene, ug/L 1,2-Trans-Dichloroethylene, μg/L 1,1,1-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L Trichloroethylene, μg/L Trichloroethylene, μg/L Vinyl Chloride, μg/L (10 (10 (10 (10 (10 (10 (10 (1	Methyl Chloride, µg/L	<10	<10
1,1,2,2-Tetrachloroethane, μg/L <10	Mathylene Chloride, pg/L	500	. 110
Tetrachloroethylene, μg/L Toluene, μg/L 1,2-Trans-Dichloroethylene, μg/L 1,1,1-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L Trichloroethylene, μg/L Trichloroethylene, μg/L Vinyl Chloride, μg/L (10 (10 (10 (10 (10 (10 (10 (1		<10	<10
Toluene, ug/L 1,2-Trans-Dichloroethylene, ug/L 1,1,1-Trichloroethane, μg/L 1,1,2-Trichloroethane, μg/L Trichloroethylene, μg/L Vinyl Chloride, ug/L (10 (10 (10 (10 (10 (10 (10 (1		<10	<10
1,2-Trans-Dichloroethylene, μg/L <10 <10 1,1,1-Trichloroethane, μg/L 180 27 1,1,2-Trichloroethane, μg/L <10 <10 Trichloroethylene, μg/L <10 <10 Vinvl Chloride, μg/L <10 <10		330	52
1,1,2-Trichloroethane, μg/L Trichloroethylene, μg/L Vinvl Chloride, μg/L (10 <10 <10 <10			<10
1,1,2-Trichloroethane, μg/L Trichloroethylene, μg/L Vinvl Chloride, μg/L (10 <10 <10 <10	1.1.1-Trichloroethane. ug/L	180	27
Trichloroethylene, µg/L <10 <10 Vinyl Chloride, µg/L <10 <10	· · · · · · · · · · · · · · · · · · ·		<10
Vinyl Chloride, ug/L <10 <10		<10	<10
	Vinvl Chloride, ug/L		

Unless otherwise noted, analyses are in accordance with the methods and procedures outlined and approved by the Environmental Protection Agency and conform to quality assurance protocol.

 [&]quot;Less-then" (<) values are indicative of the detection limit.

The Chester Engineers to be seen to be seen

Laboratory Analysis Report For

Bres-Lube Penn, Inc. Coraopolis, Pennsylvania

		Analyses			
Samples Received: Report Date: 9/17/85	Coolent Water	Composite of 85-6908, 6910 and 6912 Serried for 5 days and	Log No. 85-7039, pH 9.0 with Lime and 10 mg/L Sulfide and 1 g/L Activated		Log No. 85-7041 PH 9.0 with Lime and 10 mg/L Sulfide and 1 g/L Activated
Source	2 Trestment	Oil Skimmed	Clay Added	011 Skimmed	Clay Added
Log No. 85-	6913	7039	7040	7041	7042
Date Collected	8/22/85	:	:		•
H a	3.9	2.1	8.5	4.4	
BODs. mg/L	2,270	3,050	3,400	3,015	3,
Freon Extractables, mg/L	128	170	26	63	55
Phenolics, mg/L PhOH	3.7	19	17	17	16
Ammonia, mg/L N	52	121	101	140	146
Cyanide, mg/L CN	<0.01	<0.01	10.0>	(0.0)	10.0>
Chromium, mg/L Cr	0.11	0.09	<0.01	0.03	10.0>
Copper, mg/L Cu	0.23	0.43	0.02	0.06	10.0
Lead, me/L Ph		0.75	0.03	0.28	0.01
Nickel me/L Ni	0.89	0.38	0.15	0.28	0.08
Zinc, mg/L In	67	28	0.24	17	0.10

3402-90

Unless otherwise noted, analyses are in accordance with the methods and procedures builtned and approved by the Environmental
Protection Agency and conform to quality assurance protocol.
 "Less-than" (<) values are indicative of the detection limit.

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The Chester Engineers on the state of the st

Laboratory Analysis Report For

Bres-Lube Penn, Inc. Coriopolis, Pennsylvania

Analyses

8/23/85 9/17/85 Samples Received: Report Date:

Source	Emulsion Breaking Wastewater 1 Trestment	Emulsion Breaking Wastewater '2 Treatment	Dehydrated Water	Dehydrated Water	Coolant Water ol Treatment
Log No. 85- Date Collected	6908	6909 8/22/85	6910 8/22/85	6911 8/22/85	6912 8/23/85
H	6.0	5.3	5.5	5.2	1.5
BODS. mg/L	3,350	006'4	4,770	7,200	3,170
Freon Extractables, mg/L	621	19	19	ac	28
Phenolics, mg/L PhOH	15	13	38	38	4.0
Ammonta me/L N	96	141	145	146	15
Cyanide mg/L CN	0.032	0.026	<0.01	(0.01	(0.01
Chromium, mg/L Cr	_ 80.0	0.01	(0.0)	(0.01	0.27
Copper, mg/L Cu	2.0	0.03	0.01	(0.01	0.64
Lead. mg/L Pb	0.62	0.03	(0.01	(0.01	2.6
Nickel, mg/L Ni	0.48	0.36	0.01	(0.0)	1.1
Zinc, mg/L Zn	1.2	0.18	0.26	0.05	82

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Unless otherwise noted, analyses are in accordance with the methods and procedures outlined and approved by the Environmental Protection Agency and conform to quality assurance profocol.
 "Less-than" (<) values are indicative of the detection limit.

3492-90

BPDR 0002806

The Chester Engineers P.O. See 1986 Principal (1226 Principal (123 200 5700 A Division Of

Laboratory Analysis Report For

Coraopolis, Pennsylvania Bres-Lube Penn, Inc.

Analyses

9/11/85

Samples Received:

Log No. 85-6944, pH 9.0 with Log No. 85-6848 Lime and 10 mg/L 1.5 Parts, 6850- Sulfide and 1.5 Parts, 6852- 1 g/L Activated 1.0 Part, Settled Clay Added for 5 Days 6985 6986	Report Date: 9/17/85			왕*		
8/21/85 6984 6985 8/21/85	Source	Emulsion Breaking Water *2 Trestment	Composite of 85-6847, 6849 and 6851 Settled for 5 days and 0il Skimmed	Log No. 85-6984, pH 9.0 with Lime and 10 mg/L Sulfide and 1 g/L Activated Clay Added	Log No. 85-6848 1.5 Parts, 6850- 1.0 Part, Settled for 5 Days	Log No. 85-6986, pH 9.0 with Lime and 10 mg/L Sulfide and I g/L Activated Clay Added
5.2 2.0 8.4 8,250 1,500 1,400 1,400 1,22 80 218 22 12 4.3 3.8 17 (0.01 (0.01 0.01 0.01 0.01 0.02 0.01 0.01 0.01	Log No. 85- Date Collected	- :	7869	5869	9869	
8,250 1,500 1,400 218 22 22 218 22 3.6 0.1 12 4.3 3.8 111 18 117 <0.01 0.05 0.01 0.25 0.01 0.51 0.15 0.09 0.60	in G	5.2	2.0			æ.
22 80 218 22 4.3 3.8 111 111 (0.01 (0.01 (0.01 (0.01 3.0 0.15 0.07 0.08 0.07	BODs. mg/L	8,250	1,500	1,400	-	1,400
A.3 3.8 1.8 1.1 1.8 1.9 1.7 1.9 1.8 1.7 1.9 1.9 1.9 1.9 1.9 1.9 1.9 1.9 1.9 1.9	Freon Extractables, mg/L	08	218	22		·
(6.01 (6.01	Phenolics, mg/L PhOH	12	4.3	3.8	4.2	
(0.01 (0.01	Amonta, mg/L N	111	18	17	27	5.
0.01 0.05 <0.01 0.01 0.25 0.01 3.0 0.22 0.01 0.51 0.15 0.09	Cvanide, mg/L CN	<0.01	(0.0)	(0.0)	. <0.01	. <0.01
3.0 0.25 0.01 3.0 0.22 0.01 0.51 0.15 0.09	Chromium, mg/L Cr	0.01	0.05	(0.01	10.0	10.0>
3.0 0.22 0.01 0.51 0.15 0.09 0.84 0.60 0.07	Copper, mg/L Cu	0.01	0.25	0.01	0.03	(0.0)
0.51 0.15 0.09	Lead, ms/L Pb	3.0	0.22	0.01	0.47	0.03
0.07	Nickel mg/L Ni	0.51	0.15	0.09	0.13	90.0
	Zinc. mg/L Zn	78.0	09.0	0.07	0.52	90.0

BPDR 0002807

Unless otherwise noted, analyses are in accordance with the methods and procedures outlined and approved by the Environmental Protection Agency and conform to quality assurance protocol.

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The Chester Engineers P.O. Des 5244 Presidente 16224 Presidente 16224 A Division Of

Laboratory Analysis Report For

	Cor	Bres-Lube Penn, Inc. Coraopolis, Pennsylvania	nia	
Samples Received: 8/21/85 Report Date: 9/17/85		Analyses		
Source	Dehydration Water	Dehydration Water 2 Treatment	Goolant Water *1 Treatment	Coolant Water *2 Treatment
Log No. 85- Dare Collected	6847 8/21/85	6848 8/21/85	6849 8/21/85	6850 8/21/85
, Ya	- 0.9	4.2	1.4	3.1
BODS, mg/L	810	802	1,195	1,020
Freon Extractables, mg/L	176	! "	78	17
Amenotics, mg/t rhun	0.81	1.4	0.64	1.8
Cvanide, mg/L CN	0.026	0.047	<0.01	<0.01
Chromium, mg/L Gr	10.0>	10.01	90.0	0.02
Copper, mg/L Cu	0.15	40:0	90.0	0.0
Lead, mg/L Pb	0.27	0.10	0.48	0.59
Nickel, mg/L Ni	0.02	0.02	0.20	0.20
21nc, mg/L 2n	0.71	0.77	0.36	0.34

Water *1 Treatment

Bresking Emulsion

6851 8/21/85

440

<0.010.040.820.370.460.70

3482-90

Unless otherwise noted, analyses are in accordance with the methods and procedures outlined and approved by the Environmental Protection Agency and conform to quality assurance protocol.
 "Less-than" (<) values are indicative of the detection limit.

BPDR 0002808

MOON TOWNSHIP MUNICIPAL AUTHORITY

1000 Beaver Grade Road CORAOPOLIS, PA. 15108 264-4300

WATER & WATER POLLUTION CONTROL SERVICE

AUTHORITY BOARD

August 7, 1985

Leonard L. Nary, President Joseph G. Raboeky, Vice President E. R. Twigg, Secretary Gary D. Miller, Tressurer Gary A. Sheffler, Asst. Secy.-Tressurer Meyer, Darragh, Buckler, Bebenek & Eck, Solicitor Betz-Converse-Murdoch, Inc., Consulting Engineers R. W. Zollinger, P.E. General Manager

Borough of Coraopolis Municipal Building 1012 Fifth Avenue Coraopolis, PA 15108

Re:

Breslube-Penn Industrial Waste Discharge Application

Gentlemen:

Enclosed is a copy of an Industrial Waste Application submitted to the Moon Township Municipal Authority from the Breslube-Penn Corporation's Moon Township Plant. Breslube-Penn is requesting to discharge pre-treated industrial waste water into the Borough of Coraopolis Sewer System at the Groveton Pump Station. The Authority's consulting engineer, BCM Eastern, Inc., has evaluated the application and has provided the enclosed initial response for your information.

Please review the enclosed information and provide any comments to this office at your earliest convenience. Copies of this letter are also being furnished to the Coraopolis Municipal Sanitary Authority and the Allegheny County Health Department for their comments.

Thank you for your cooperation in this matter.

Very truly yours,

MOON TOWNSHIP MUNICIPAL AUTHORITY

R W Zollinger, General Manager

RWZ/sm enclosure Certified Mail #P024955719

cc: Allegheny County Health Department w/a Coraopolis Municipal Sanitary Authority w/a Township of Moon w/a MTMA Board of Directors

R. Mills, Esq. D. Nichols, PE



BCM Eastern Inc.

Engineers, Planners and Scientists

5777 Baum Blvd. • Pittsburgh, PA 15206 • Phone: (412) 361-6000

June 19, 1985

Mr. Richard W. Zollinger, General Manager Moon Township Municipal Authority 1000 Beaver Grade Road Coraopolis, Pennsylvania 15108

Subject: Industrial Wastewater Discharge Application

Breslube-Penn Inc.

BCM No. 00-3116-99, File 22(2)

Dear Mr. Zollinger:

As directed by the Authority Board at the meeting on April 17, 1985, we reviewed the information as set forth on the captioned application as amended by letter dated May 10, 1985. Our findings and comments are summarized as follows:

- Breslube-Penn operates two processes to recover and refine used lubricating oils at facilities located at 84 Montour Road near the Moon-Robinson Township border.
- Breslube-Penn proposes to discharge wastewater from the emulsion breaking process, condensate from the dehydration process, and a minimal amount of tank bottom drainage from the raw waste oil tank.
- The Chester Engineers conducted laboratory testing of two samples of raw wastewater from each process and results were submitted with the application by Breslube-Penn. Test results from additional analyses of raw and pretreated wastewater (laboratory bench) were submitted as a supplement to the original application. Tabulations of the test data have been attached (Exhibits 1 and 2) for the dehydration and emulsion breaking wastes.
- A maximum flow rate of 20,000 gpd is projected with 75% of the wastewater resulting from the dehydration process.

A Member Firm of Ref	 Converse Murdoch • Inc. 	
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Mr. Richard W. Zollinger June 19, 1985 Page 2

After review of the information submitted by Breslube-Penn, acceptance of the industrial discharge into the public system is not recommended unless reliable pretreatment is provided. Pretreatment is necessary to reduce concentrations of ammonia, oil and grease, copper, lead, nickel, and zinc.

Additional information relative to the trestability of the wastewater has been reviewed and our comments are as follows:

- Pretreatment involving flow equalization, pH adjustment with lime, sodium sulfide addition, mixing, and filtration was proposed by Chester Engineers prior to discharge to the public sewer system.
- The industrial discharge from Breslube-Penn must comply with the Rules and Regulations Governing Sewage Service published by the Moon Township Municipal Authority and Coraopolis Municipal Sanitary Authority, in addition to Pretreatment Standards for the Petroleum Refining Category promulgated by US EPA. A summary of the discharge analyses and most stringent discharge limitations has been attached (Exhibit 3).

If the profile of pretreated wastewater can be achieved continuously, the industrial wastewater could be discharged to the public sewer system for disposal. We cannot determine the reliability of the proposed pretreatment system from the preliminary treatability study. The information provided is not sufficient to recommend approval of the Preslube-Penn application for the following reasons:

- The profile of the wastewater used to evaluate the pretreatment suitability contained substantially lower concentrations of ammonia, copper, cyanides, lead, nickel, and zinc than the other samples.
- Removal percentages indicated by comparison of the raw and pretreated samples are insufficient to reduce toxic metal levels to acceptable values. Certification is needed from the designer that the proposed pretreatment will remove the prohibited contaminants and guarantee from owner that the system will be operated to preclude unacceptable wastes.
- The range of concentrations indicated a wide variation in the wastewater. An acceptable pretreatment system would be required to protect the public system from discharge of prohibited wastewater at all times. Therefore, the system must be capable of handling the toughest wastes.



Mr. Richard W. Zollinger June 19, 1985 Page 3

- No analysis was submitted for the tank bottom drainings from the raw oil feed unit.
- In view of the fact that the Breslube-Penn wastewater could be conveyed through the Montour Run pump station, precautions must be taken to preclude the collection of light oils in the wet well for safety reasons.

Despite our concerns regarding the acceptability of the pretreated wastewater, we have preliminarily reviewed the magnitude of charges to assist Breslube-Penn in the evaluation of constructing onsite treatment facilities versus discharging to the public system.

Based on the discharge of 20,000 gallons per working day and a six-day work week, the estimated cost of transporting and treating wastewater from Breslube-Penn will require recovery of the following costs:

· User charges payable to MTMA include the standard charge according to the rate schedule and the CMSA surcharge for treatment based on the average strength (BOD $_5$) of weekly composite samples.

MTMA Base Charge = $(520,000 \text{ gal/mon}) \times (\$1.29/1,000 \text{ gal}) \times 12$ = \$8,000/yr.

CMSA Surcharge = $(520,000 \text{ gal/mon}) \times (\$1.94/1,000 \text{ gal}) \times 0.001 \times (1356-250) \times 12 = \$13,400/yr.$

 Costs for transportation of the wastewater via the Montour Run pump station will be imposed by CMSA.

CMSA Transportation Charge = $(520,000 \text{ gal/mon}) \times (\$0.08/1,000 \text{ gal}) \times 12 = \$500/yr.$

 Costs of composite sampling, testing, and monitoring operation of the pretreatment system would also be recovered by MTMA.

Industrial Cost Recovery = (60 samples/yr.) x (\$200/sample) =
\$12,000/yr.

Total charges would be on the order of \$33,900 per year. In addition, Breslube-Penn would be responsible for all costs of constructing and operating pretreatment facilities.



Mr. Richard W. Zollinger June 19, 1985 Page 4

In summary, we do not recommend approval of the proposed discharge of industrial wastewater without proper assurance that adequate pretreatment will be provided continuouly and the system is protected from accidental spills that would endanger personnel and operations. Any agreement to accept industrial wastes must include proper clauses and remedies to enforce compliance.

Should you have any questions regarding this matter, please do not hesitate to call.

Very truly yours.

David G. Nichols, P.E. Assistant Vice President

DGN/dc Enclosures

cc: Richard J. Mills, Esquire (w/enc.)

450

APPLICATION REQUESTING SERVICE FOR

INDUSTRIAL WASTEWATER DISCHARGE

TO

MOON TOWNSHIP MUNICIPAL AUTHORITY

1000 Beaver Grade Road Coraopolis, PA 15108

APPLICATION NO		•	DATE:	•
Application is here	by made by	BRESLUBE-PE (Print or Type	NN, INC.	on.
(Mailing Address)	84 Montour Ro	oad Coracpol	is, PA	15108
	(Street)	(City)	(State)	(Zip)
, **	•	ħ,	i.	
for permission to d	ischarge wast			he Moon Township
Municipal Authority	facilities f	rom Bresl	ube-Penn. Inc.	
(Print or	Type Owner, T	enant Name Di	oducing Wast	on the
property located a	t 84 Mantou	r Road Cor	sopolis, PA	15108
	(Street)	(City)	(State	(Z1p)
,		•		
1. Type of Industr	y: Re-refine	r of lubrication	g oils	
•	,	General Desci	ription)	
2 Fodoral SIC No.	2992			·
2. Federal SIC Nos			<u> </u>	
3. Raw Material Us	ed: Used	lubricating oil	5	
	(General I	escription-A	dd Additional	Sheets as Necessa
4. Products Produc	ed: Re-re	fined lubricati	ng oil and fuel	oil
	(General I	escription-Ad	d Additional	Sheets as Necessa
			· .	
5. Wastewater Prod	ucing Operati	lons: See	Attachment	
			_	
(Eul) Decerie	tion - Add Ad	iditional She	ate as Nacass	2

6.	Number of	Employees:	13	Full Time/	Pa	rt Time
rime	e of Discha	arge: 12 AM, (Working I	/BM to 12 Day - Cro	XXWPM Days	per Week: PM)	s MT(W) F(S) (Circle Days)
8.	Wastewate	r Flow Rate:	20,000 =	aximum ga	llons per da	Y
9.	Constitue	nts of Wastewai	ter Disch	arge:	See Attachment	
	(Genera	al Description	- Attach	Chemical And	alyses to Ap	plication)
0.	Pretreatme	ent Facility:_		See a	tachment	·
			·	·		
		(Genera	al Descri	ption - If P	roposed)	
ι1.	Person in	company respon	nsible fo	r industrial	wastewater	discharge:
	Ahsen Yelk	in		Vice Presiden (Posit	t of Operation	264-4280
		(Name)		(Posit	ion)	(Telephone)
Iai		all information	on furnis	hed is true	and correct	and that the
app:	licant will	comply with	the Rules	and Regulat	ions of the	Moon Township
	icipal Auth	-	Signa	ture of Appl	icant:	mulley 3
·	<i>i.</i> .		Posit	ion of Signe	e: Vice Presi	ient of Operations
	Use By	Date	Received		Date Res	viewed
	Moon nship	Revi	ewed by:	•		
	icipal hority			(Name)	{Pc	sition)
AUG	y	Acti	on Recomm	ended:		
	•					
		1.	•			,
		1 - · · ·				

WASTEWATER PRODUCING OPERATIONS AND CHARACTERIZATION OF WASTEWATER

Breslube-Penn, Inc, located in Hoon Township, Allegheny County, PA, re-refines used lubricating oils utilizing a number of processes. Used oil is brought into the plant and unloaded into a used oil storage tank. From this storage tank the used oil is either pumped to a dehydration process or to a chemical emulsion breaking process depending on the used oil quality. If the used oil has a bottom sediment and water (BS&W) content greater than 93%, it is pumped to the chemical emulsion breaking process. All other used oil is pumped to the dehydration process.

The dehydration process consists of interjecting the waste oil into a large boiler. The boiler is equipped with steam coils which are supplied with 100-125 psig steam. The used oil is heated to approximately 240°F. At this temperature water and "light end" hydrocarbons are boiled off and subsequently condensed at an overhead condenser. The condensate is then drained to an API separator to separate the water from the light ends. The water portion is presently discharged through two more API separators to Montour Run.

The chemical emulsion breaking process is presently utilized by Breslube for treating the used oil with a BS&W content greater than 93%. The process involves ph adjustment and the addition of an oil emulsion breaking chemical into an agitated vessel. After thorough mixing, the solution is allowed to sit in a quiescent state for a period of over 24 hours. This allows the less than 7% oil fraction to separate from the water portion. The remaining water is then drained through two API separators to Montour Run. The oil portion is sent on to the dehydration process for further oil/water separation.

The wastewater stream which Breslube proposes to discharge to the Corsopolis sewerage system consists of the water from the dehydration system, the water from the emulsion breaking process and a minimal amount of tank bottom drainings. The tank bottom drainings are the bottom few hundred gallons of a raw waste oil feed

tank. This portion is the water that has separated from the oil while the feed tank was being pumped to the processing system. This source contributes approximately 100 gallons per day of wastewater.

The westewater is presently discharged into Montour Run under NPDES permit number PA0044695. A review of the Discharge Monitoring Reports (DMR) for the period from September 1983 through November 1984 has revealed the following effluent characteristics:

Parameter	Maximum	Average Haximum
Oil and Grease	41 mg/L	24.3 mg/L
Ammonia Nitrogen	32.4 mg/L	18.4 mg/L
BOD5	2,300 mg/L	1,356 mg/L
Phenol	35 mg/L	18.3 mg/L
PH	7.0 max, 5.4 min.	5.83 avg. min.
Flow	0.02 mgd	0.014 mgd
Total Suspended Solids	268 mg/L	102.15 mg/L
Copper	0.31 mg/L	0.08 mg/L
Zinc	1.50 mg/L	1.15 mg/L
Lead	0.45 mg/L	0.168 mg/L
Chromium	1.75 mg/L*	less than 0.27 mg/L
Cyanide	80.0	less than 0.03 mg/L
Nickel	0.56	0.22 mg/L
Temperature	121	104

^{*}includes Hexavalent Chromium only

Breslube was discharging in violation of its NPDES permit for the 15 month period reviewed. The violations were mainly on phenols and BODs.

Breslube is addressing the elimination of these violations by looking at two alternatives. One would be to construct an activated sludge type of biological treatment plant on-site for continued discharge to Montour Run. Experience with this type of treatment at the Breslube-Canada facility has shown that 92 percent

reduction of BOD and 98.5 percent reduction of phenol concentrations can be achieved by such treatment. Breslube has submitted an application to DER for approval of plans to implement this alternative.

The other alternative, which we are addressing here, is to pretreat the wastewater and discharge it to the Coraopolis severage system. Under this alternative, the wastewater would need to be pretreated to ensure that it meets the standards of the USEPA, the Moon Township Municipal Authority and the Coraopolis Municipal Sanitary Authority.

Breslube's operation places them into the USEPA's Petroleum Refining-Lube Subcategory. The Pretreatment Standards for existing sources for that Subcategory, as revised on October 18, 1982, to discharge into a Publicly Owned Treatment Works, are as follows:

Pollutant	Maximum For Any One Day
Oil and Grease	100 mg/L
Ammonia (N)	100 mg/L

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The Coreopolis Ordinance governing discharge to their Sewage Disposal System includes the following prohibitions:

Parameter	<u>Maximum</u>			
рН	between 5.5 and 9.0			
Temperature	150°F			
Oil and Grease	100 mg/L			
Copper	0.1 mg/L			
Zinc	0.5 mg/L			
Lead	0.1 mg/L			
Boron	1.0 mg/L			
Chromium	3.0 mg/L			
Nickel	0.5 mg/L			
Cyanides	2.0 mg/L			
Sodium Chloride	10,000 mg/L			
Free Oil	50 mg/L			

The Moon Township Municipal Authority's guidelines limit the following specific constituents:

Parameter	Maximum
Temperature	100°F
Oil and Grease	120 ррш
pH .	between 6.5 and 9.0

A comparison of the Breslube effluent quality presented in the DMR's with the USEPA and Coraopolis pretreatment standards indicated that pretreatment would be required for removal of lead, zinc, copper and nickel. In order to develop a pretreatment process that would ensure compliance with the regulations, samples were obtained from Breslube and analyzed and treatability studies were performed. One immediate conclusion that was drawn through such sampling and analysis was that the raw wastewater quality varied significantly from that reflected in the DMR's. The raw wastewater quality found was as follows:

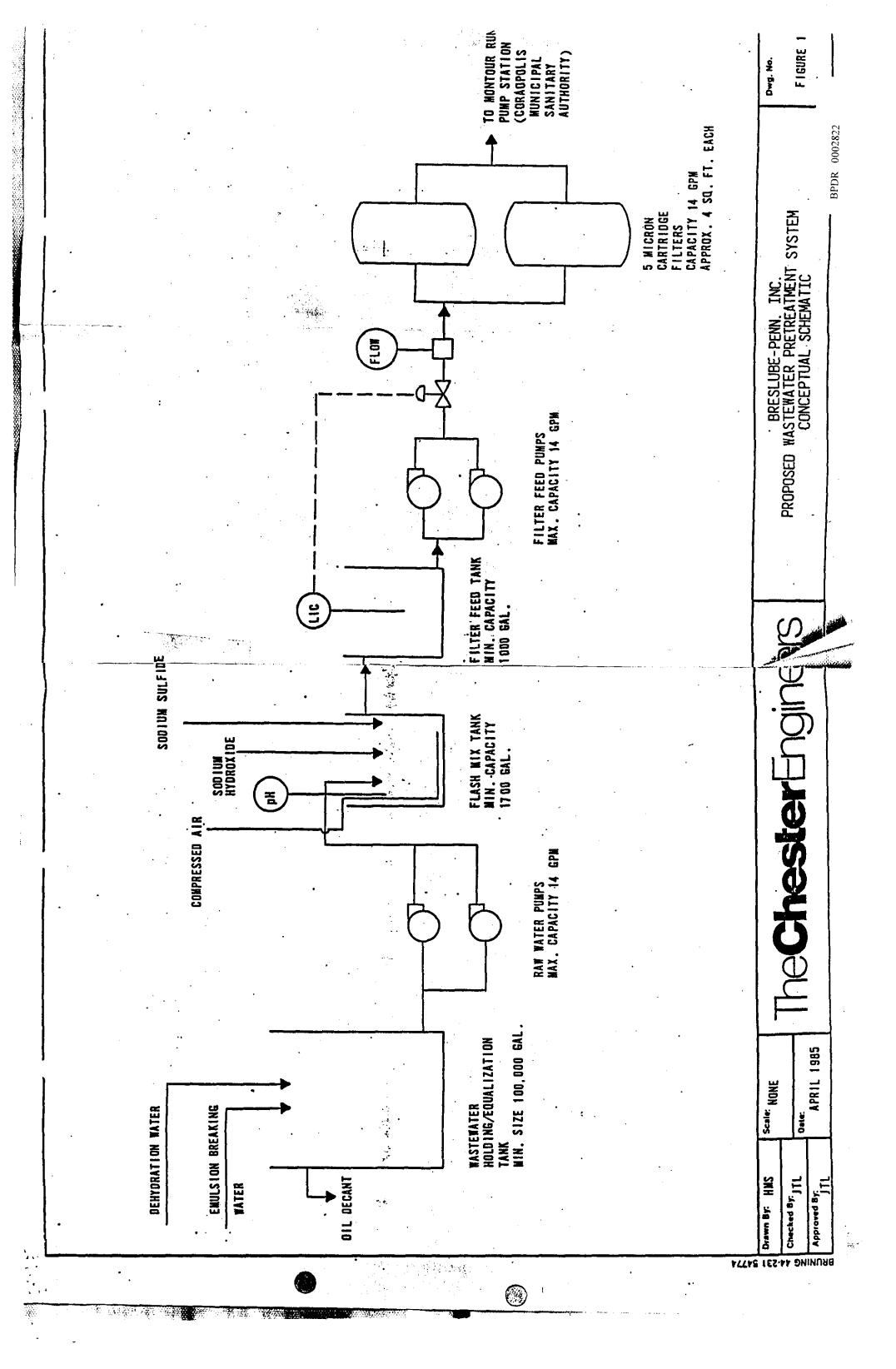
Source	Dehydration	Water	Emulsion !	Breaking Water	
	Concentration				
	2/9/85 Grab	3/13/85 24-hr Comp.	2/9/85 Grab	3/29/85 Grab	
Ammonia (N) mg/L	174		117 .		
Oil and Grease mg/L	32	502	230	877	
Total Cyanide mg/L	1.0	less than 0.0005			
Total Chromium les	s , than , 0 . 01	0.01	0.02	0.01	
Copper mg/L	0.32	0.08	0.06	0.06	
Lead mg/L	1.2	0.60	0.24	0.08	
Nickel mg/L	0.03	0.11	0.38	0.21	
Zinc mg/L	:14	1.6	3.0	0.74	
рH	5.2		6.2		

From these analyses, it was obvious that treatment would be necessary to lower the Ammonia, Oil and Grease, Copper, Lead, Zinc and Nickel concentrations as well as to raise the pH. "After several trials the treatment scheme shown on Figure 1 was shown to be the most cost-effective in producing the desired effluent quality. The process will be as follows.

Wastewater from the existing processes will be routed through an API separator and pumped to an equalization/holding tank. This tank will be capable of holding a minimum of five days of wastewater flow. The wastewater will be pumped from this tank for continuous treatment on a 24 hour per day, 7 days per week basis. The treatment scheme will be designed to handle a maximum flowrate of 20,000 gallons per day.

The treatment scheme will consist of adding liquid sodium hydroxide into the wastewater in a flash mix tank using a pH controlled, variable volume chemical feed pump. The pH will be controlled to pH 9. Approximately 10 mg/L of sodium sulfide will be added to further form precipitates with the metal ions. The tank will be agitated using compressed air to effect some stripping of the ammonia. A detention time of approximately two hours will be provided. The waste stream will then overflow into a filter feed tank from which it would be pumped at a constant rate through one of two 5 micron cartridge filters. The filters will remove the precipitates formed in the flash mix tank as well as the insoluble oil and grease and other suspended matter. The flowrate through the filter would be metered and sampled using an automatic composite sampler. The "on-line" filter would be switched when the pressure drop through the filter, as indicated on influent and effluent pressure gauges, exceeds a predetermined value. The spent cartridges would be disposed of in an environmentally safe manner as necessary. The resultant discharge will be within the effluent quality limitations presented herein. Additional treatability studies to verify the dependability of the treatment scheme selected are being performed by Chester. The results of these studies will be issued when available. If modifications to the treatment process presented herein are required as a result of the confirmation studies, an addendum to this report will be issued.

To summarize, the proposed discharge will be a continuous 24 hour per day, 7 days per week discharge at a maximum flowrate of 20,000 gallons per day. The effluent concentrations after treatment will be within the pretreatment limitations promulgated by the various regulatory agencies. The wastewater will contain relatively high concentrations of BOD and phenol which are amenable to the treatment process provided at the Coraopolis Sewage Treatment Plant. The introduction of these pollutants into the plant is not expected to affect the plant's ability to provide the treatment efficiency required to ensure compliance with its NPDES permit. Such introduction is also not expected to affect the characteristics of the sludge which allow it to be disposed of in a landfill.



MOON TOWNSHIP MUNICIPAL AUTHORITY

1000 Beaver Grade Road CORAOPOLIS, PA. 15108 264-4300

WATER & WATER POLLUTION CONTROL SERVICE

AUTHORITY BOARD

Leonard L. Nary, President Joseph G. Rebosky, Vice President E. R. Twigg, Secretary Gary D. Miller, Treesurer Gary A. Shefiler, Asst. Secy.-Treesurer

November 5, 1985

Meyer, Darragh, Buckler,
Bebenek & Eck, Solicitor
Betz-Converse-Murdoch, Inc.,
Consulting Engineers
R. W. Zollinger, P.E.
General Manager

Borough of Corsopolis Municipal Building 1012 Fifth Avenue Corsopolis, PA 15108

Re: Breslube-Penn Industrial Waste Discharge Application

Gentlemen:

Enclosed is some supplemental information relative to the referenced industrial waste discharge application for your review. As previously indicated by our August 7, 1985 correspondence, the Breslube-Penn Corporation is requesting to discharge their pretreated industrial waste water into the Borough of Corsopolis' sewer system at the Groveton Pump Station.

Before the Authority can act on their application, we have to obtain the Borough of Coraopolis' comments and/or approval regarding the acceptability of this industrial waste.

Please contact me at 264-4300 should you have any questions regarding this request.

Very truly yours,

MOON TOWNSHIP MUNICIPAL AUTHORITY

Zollinger, General Manager

RWZ/sm enclosures

cc: ACHD - all w/a

CHSA

MTMA Board of Directors

R. Mills, Esq.

D. Nichols, PE

Coraopolis Municipal Sanitary Authority

BOROUGH BUILDING CORAOPOLIS, PENNA. 15108 Phone, 264-3002 January 20, 1986

R. W. Zollinger, General Manager Moon Township Municipal Authority 1000 Beaver Grade Road Coraopolis, PA 15108

Breslube-Penn Industrial Waste Discharge Application

Dear Mr. Zollinger:

This is in answer to your letter of November 5, 1985 concerning the industrial waste of the above applicant.

The directors of the Corsopolis Municipal Sanitary Authority considered the request at their recent meeting and were unable to approve it. The problem from the directors standpoint seems to be the extension of the service lines and the opening of a new service area in addition to the problem of the industrial waste.

Very truly yours,

CORAOPOLIS MUNICIPAL SANITARY AUTHORITY

President